

15th Specialized Conference on
Small Water & Wastewater Systems

7th Specialized Conference on
Resources Oriented Sanitation



Dynamic membrane for particle removal with large pore size mesh in wastewater treatment

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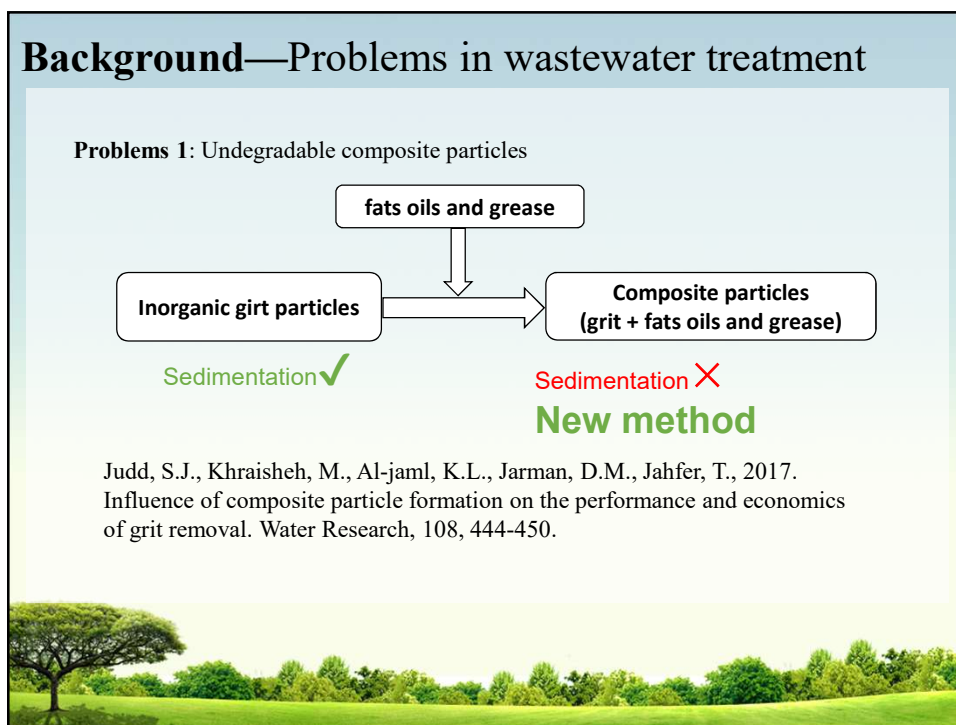
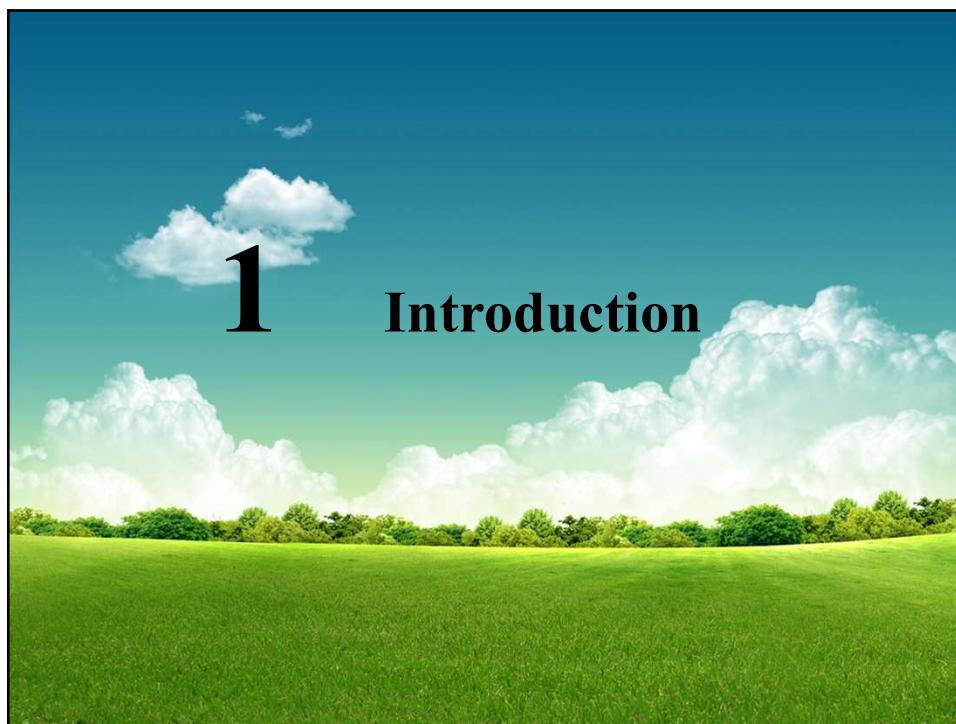
Outline

1. Introduction

2. Material & Method

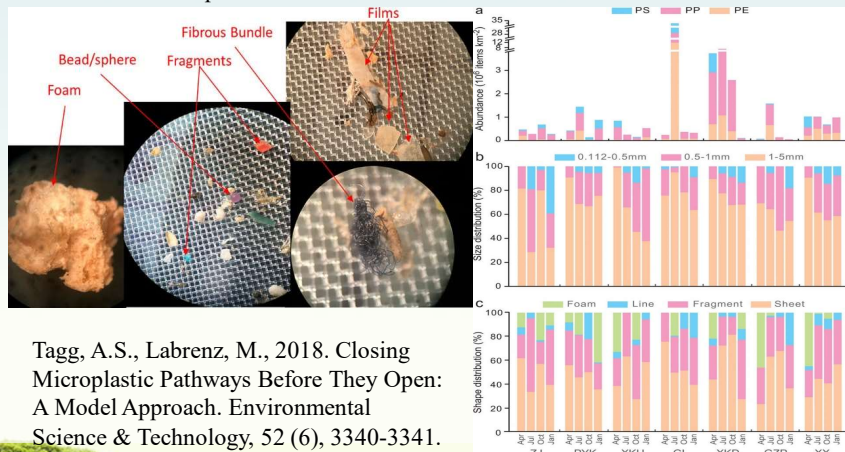
3. Results

4. Conclusion

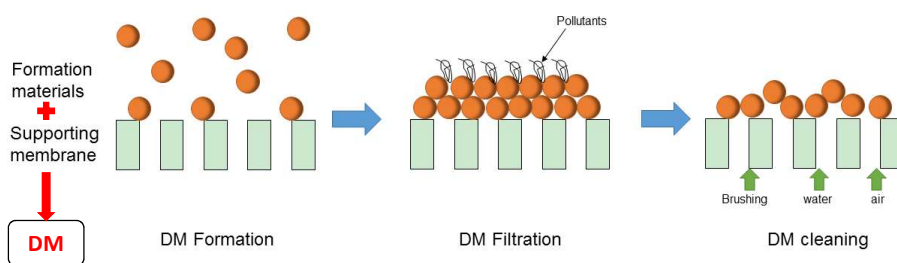


Background—Problems in wastewater treatment

Problems 2: Microplastics in wastewater

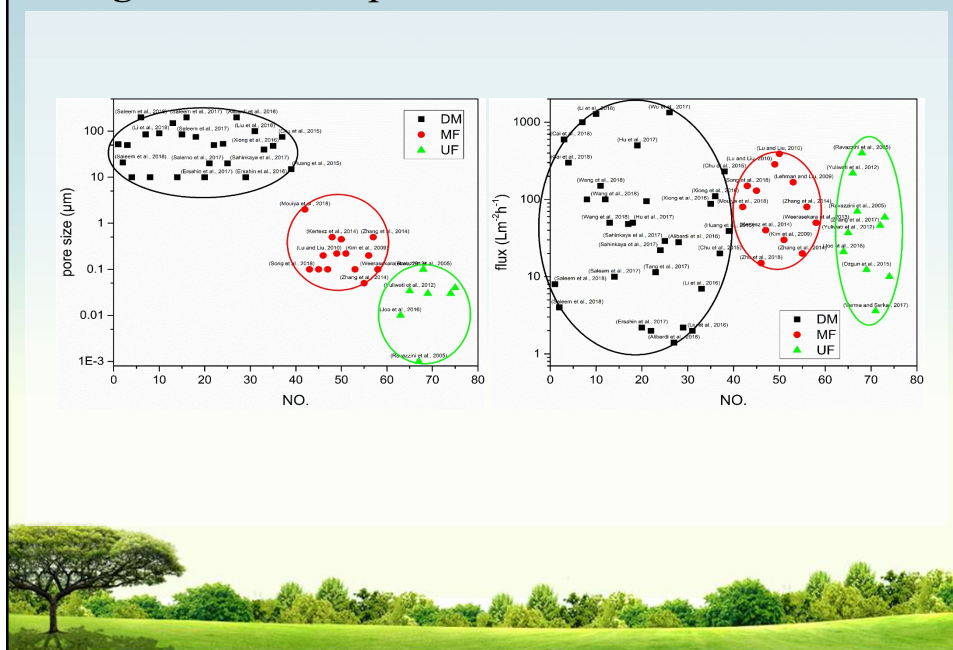


Background—Dynamic membrane technology

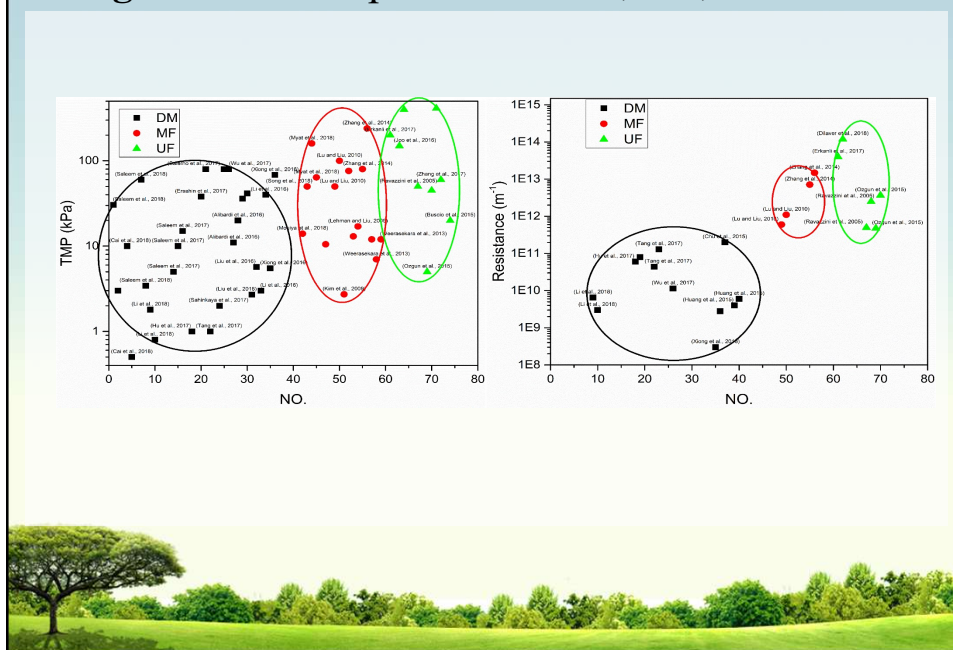


Li, L., Xu, G., Yu, H., 2018. Dynamic Membrane Filtration: Formation, Filtration, Cleaning, and Applications. *Chemical Engineering & Technology*, 41 (1), 7-18.

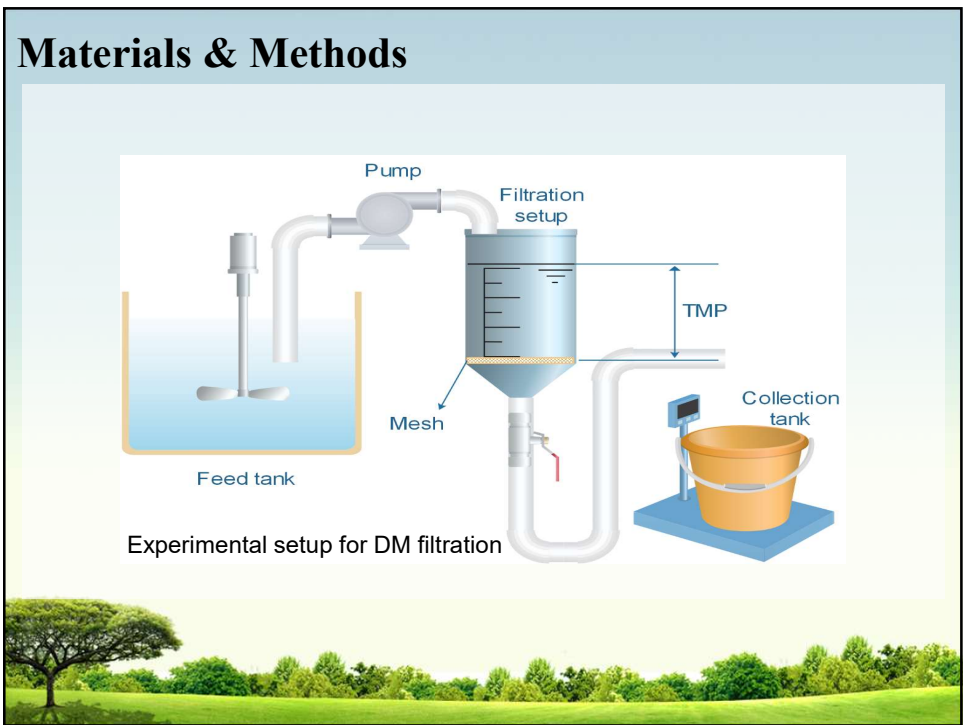
Background—Comparison of DM, MF, UF



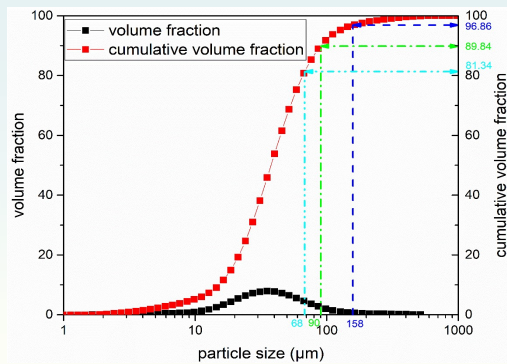
Background—Comparison of DM, MF, UF



2 Materials & Methods



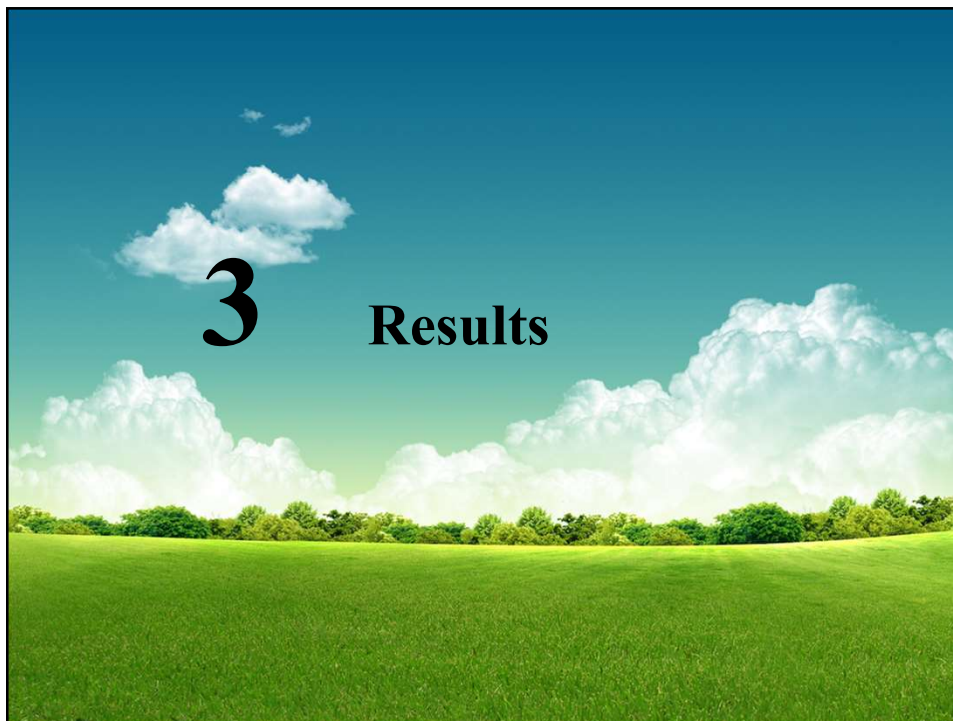
Materials & Methods



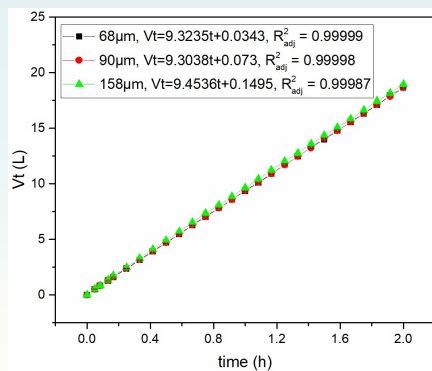
The relationship between particle size distribution and mesh pore size



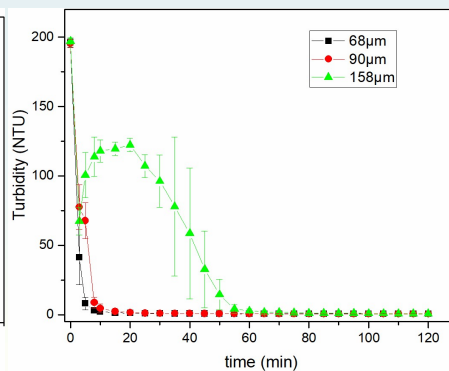
3 Results



Results—Effluent volume



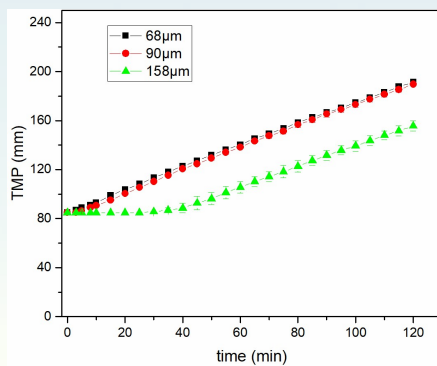
Variation of effluent volumes with different pore size meshes



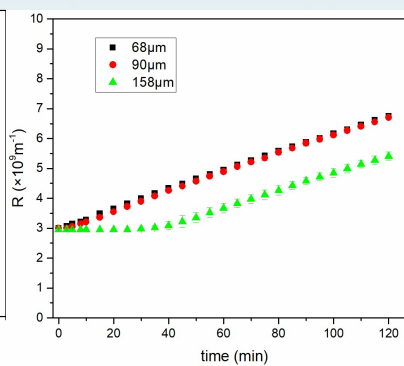
Variation of effluent turbidity with different pore size mesh



Results—TMP & filtration resistance

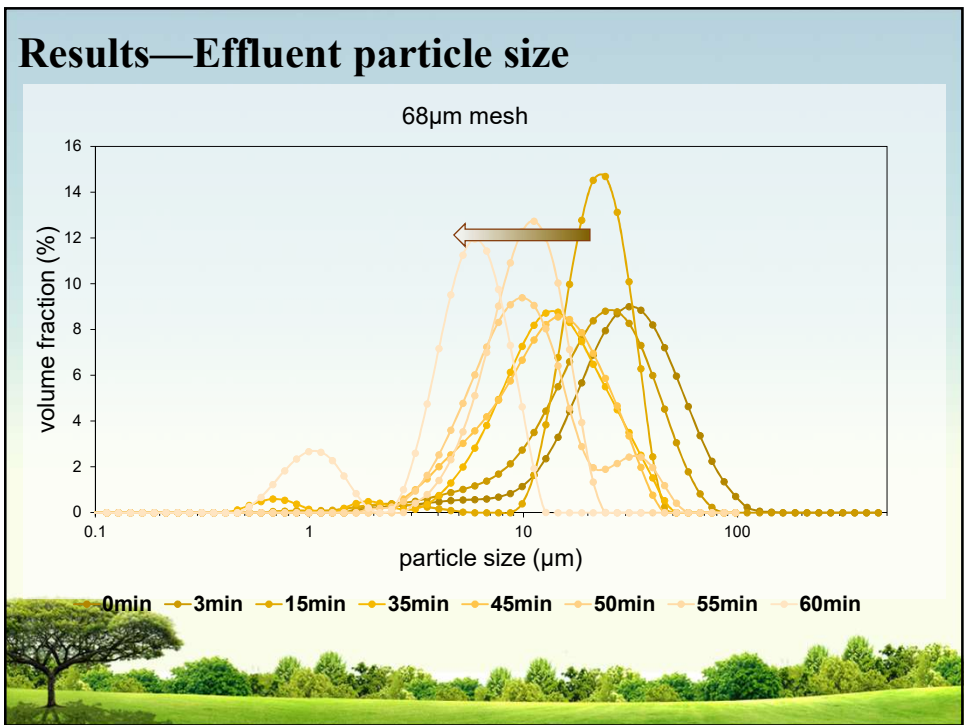
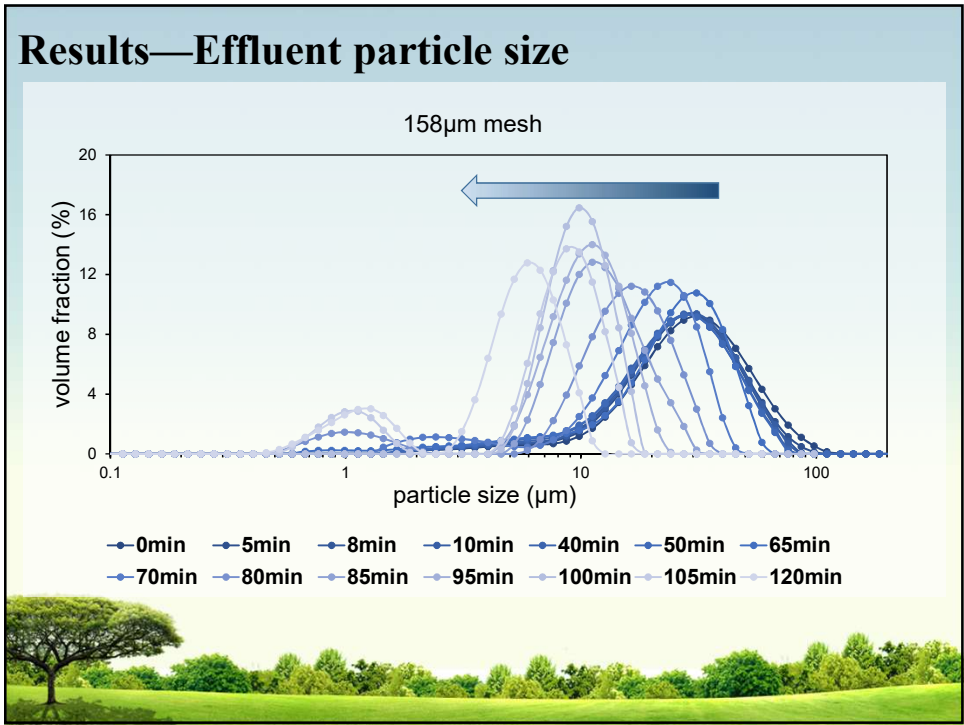


Variation of TMP with different pore size mesh



Variation of filtration resistance with different pore size mesh

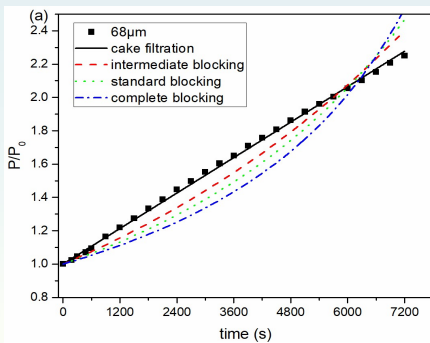




Results—DM formation mechanism

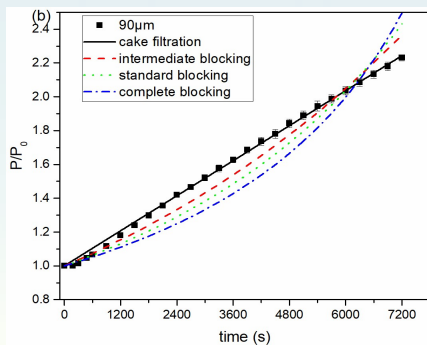
Blocking mechanism	Model equation	Blocking constant
Cake filtration	$\frac{P}{P_0} = 1 + K_c J_0^2 t$	K_c
Intermediate blocking	$\frac{P}{P_0} = \exp(K_i J_0 t)$	K_i
Standard blocking	$\frac{P}{P_0} = \left(1 - \frac{K_s J_0 t}{2}\right)^{-2}$	K_s
Complete blocking	$\frac{P}{P_0} = \frac{1}{1 - K_b t}$	K_b
Cake-complete blocking	$\frac{P}{P_0} = \frac{1}{(1 - K_b t)} \left(1 - \frac{K_c J_0^2}{K_b} \ln(1 - K_b t)\right)$	K_b, K_c
Cake-intermediate blocking	$\frac{P}{P_0} = \exp(K_i J_0 t) \left(1 + \frac{K_c J_0}{K_i} (\exp(K_i J_0 t) - 1)\right)$	K_i, K_c
Complete-standard blocking	$\frac{P}{P_0} = \frac{1}{(1 - K_b t) \left(1 + \frac{K_s J_0}{2 K_b} \ln(1 - K_b t)\right)^2}$	K_b, K_s
Intermediate-standard blocking	$\frac{P}{P_0} = \frac{\exp(K_i J_0 t)}{\left(1 - \frac{K_s}{2 K_i} (\exp(K_i J_0 t) - 1)\right)^2}$	K_i, K_s
Cake-standard blocking	$\frac{P}{P_0} = \left(1 - \frac{K_s J_0 t}{2}\right)^{-2} + K_c J_0^2 t$	K_s, K_c

Results—Single blocking model



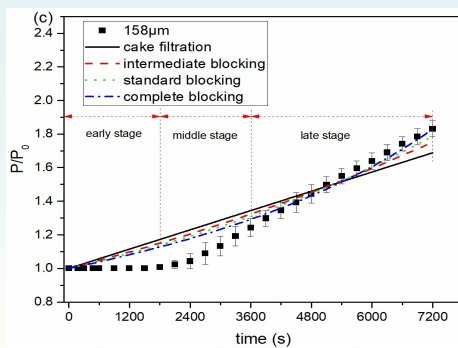
Mesh	Parameters	Cake filtration	Intermediate blocking	Standard blocking	Complete blocking
68µm	K	1448.11	0.35	0.29	8.41×10^{-5}
	Standard error	5.51	0.00539	0.00551	1.78×10^{-6}
	R_{adj}^2	0.99876	0.96094	0.91466	0.84543
	RMSE	0.01418	0.07969	0.1178	0.15853

Results—Single blocking model



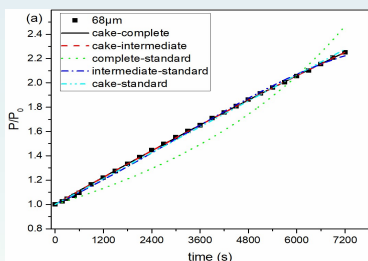
Mesh	Parameters	Cake filtration	Intermediate blocking	Standard blocking	Complete blocking
90µm	K	1409.34	0.34	0.28	8.33×10^{-5}
	Standard error	7.18	0.00456	0.00491	1.63×10^{-6}
	R_{adj}^2	0.99794	0.97318	0.93579	0.87715
	RMSE	0.01847	0.06657	0.10301	0.142

Results—Single blocking model



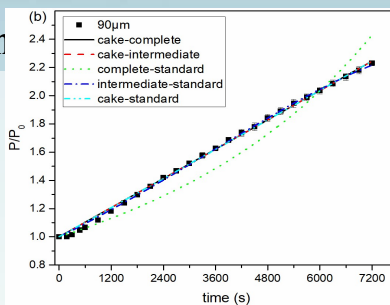
Mesh	Parameters	Cake filtration	Intermediate blocking	Standard blocking	Complete blocking
158µm	K	780.67	0.22269	0.20036	6.29×10^{-5}
	Standard error	41.21	0.00745	0.00515	1.22×10^{-6}
	R_{adj}^2	0.8684	0.91495	0.93458	0.94992
	RMSE	0.10604	0.08525	0.07477	0.06542

Results—Combined blocking model

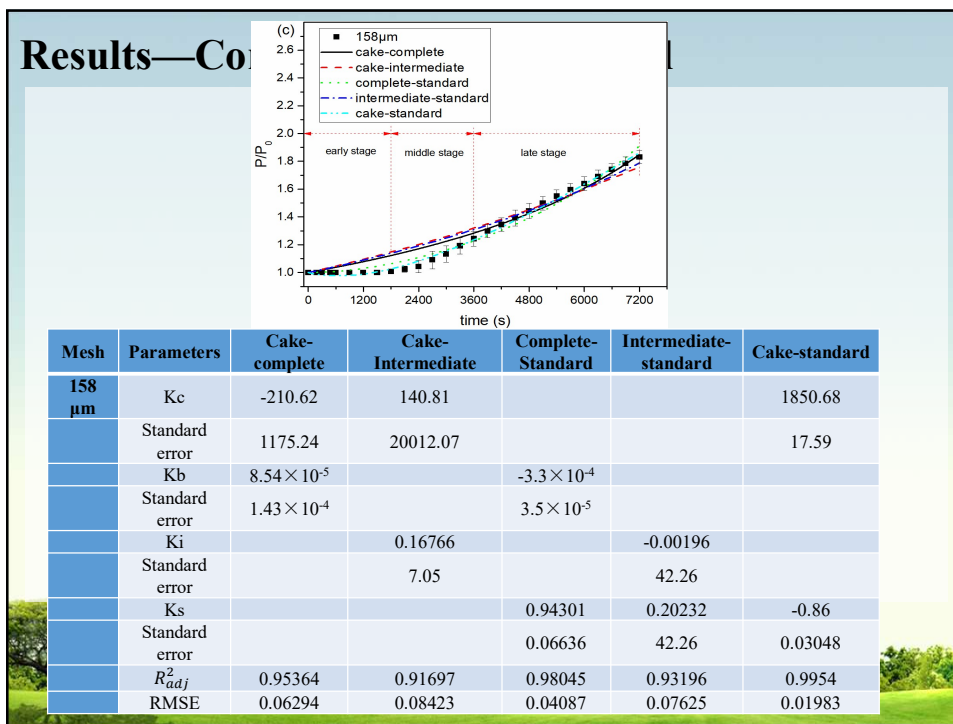


Mesh	Parameters	Cake-complete	Cake-Intermediate	Complete-Standard	Intermediate-standard	Cake-standard
68µm	Kc	1611.86	1607.84			1448.10
	Standard error	18.88	17.85			2.19×10^6
	Kb	-8.02×10^{-6}		3.3×10^{-8}		
	Standard error	9.04×10^{-7}		0.00254		Over Parameterized
	Ki		-0.02192		-0.60566	
	Standard error		0.00234		0.00758	
	Ks			0.29	1.06381	3.42×10^{-6}
	Standard error			7.24	0.01161	765.19
	R_{adj}^2	0.9997	0.9997	0.91124	0.99865	0.99871
	RMSE	0.00701	0.00698	0.12013	0.01484	0.01446

Results—Com



Mesh	Parameters	Cake-complete	Cake-Intermediate	Complete-Standard	Intermediate-standard	Cake-standard
90µm	Kc	1399.06	1398.91			1541.36
	Standard error	48.42	48.60			202.69
	Kb	5.20×10^{-7}		8.9×10^{-7}		
	Standard error	2.42×10^{-6}		0.00476		Over Parameterized
	Ki		0.00151		-0.56786	
	Standard error		0.00696		0.00794	
	Ks			0.28218	1.0025	-0.0495
	Standard error			13.58	0.01194	0.08144
	R_{adj}^2	0.99786	0.99786	0.93322	0.99874	0.99786
	RMSE	0.01882	0.01882	0.10505	0.01444	0.0188



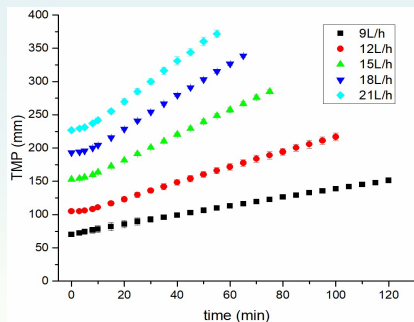
Results—Model evaluation

Mesh	Function	Status	AIC	BIC
68µm	Cake-intermediate CF	Succeeded	-263.12658	-260.28255
	Cake-complete CF	Succeeded	-262.92686	-260.08282
	Cake filtration CF	Succeeded	-226.33783	-224.24615
	Intermediate-standard CF	Succeeded	-222.40509	-219.56106
	Intermediate CF	Succeeded	-133.11795	-131.02627
	Standard CF	Succeeded	-112.01331	-109.92163
	Complete-standard CF	Succeeded	-109.46979	-106.62576
	Complete CF	Succeeded	-95.97713	-93.88546
	Cake-standard CF	Failed		
	90µm	Cake-intermediate CF	Succeeded	-223.8692
Cake-complete CF		Succeeded	-212.07087	-209.97919
Cake filtration CF		Succeeded	-209.57933	-206.7353
Intermediate-standard CF		Succeeded	-209.5787	-206.73467
Intermediate CF		Succeeded	-209.56119	-206.71715
Standard CF		Succeeded	-142.8288	-140.73713
Complete-standard CF		Succeeded	-119.2586	-117.16693
Complete-CF		Succeeded	-116.71513	-113.8711
Cake-standard CF		Failed		
158µm		Cake-standard CF	Succeeded	-158.68458
	Complete-standard CF	Succeeded	-148.85797	-146.01393
	Complete CF	Succeeded	-143.7763	-141.68462
	Cake complete CF	Succeeded	-144.37774	-141.53371
	Standard CF	Succeeded	-136.55993	-134.46826
	Intermediate standard CF	Succeeded	-134.01645	-131.17242
	Intermediate CF	Succeeded	-129.47622	-127.38454
	Cake-intermediate CF	Succeeded	-128.64064	-125.79661
	Cake filtration CF	Succeeded	-117.69099	-115.59932

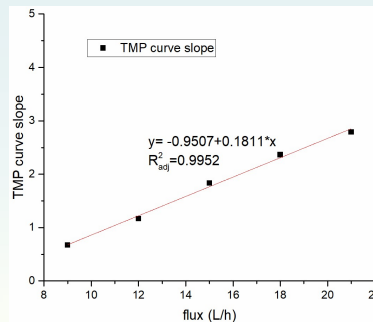
AIC: Akaike information criterion, an estimator of the relative quality of statistical models for a given set of data. Thus, AIC provides a means for model selection.

BIC: Bayesian Information Criteria, a criterion for model selection among a finite set of models; the model with the lowest BIC is preferred.

Results—Influencing factors—influent flow



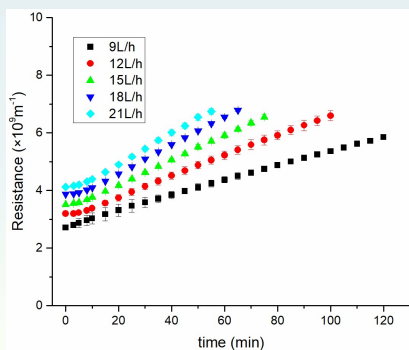
Variation of TMP with time under different influent flow



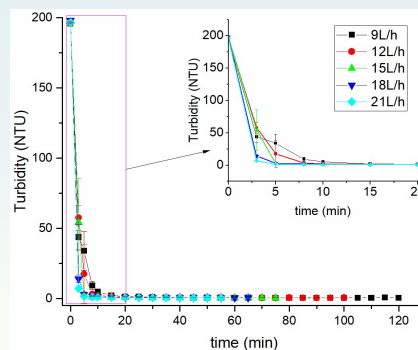
Variation of TMP curve slope with different influent flow



Results—Influencing factors



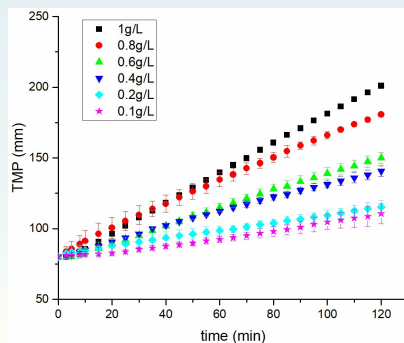
Variation of filtration resistance with time under different influent flow



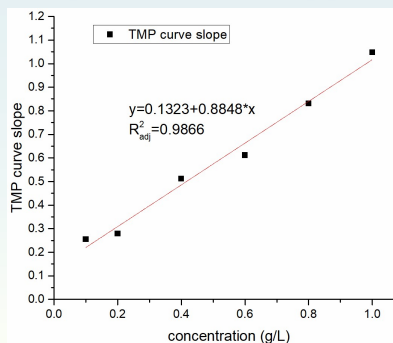
Variation of effluent turbidity with time under different influent flow



Results—Influencing factors—influent particle concentration



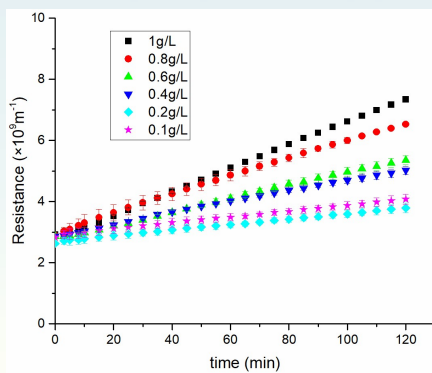
Variation of TMP with time under different influent particle concentration



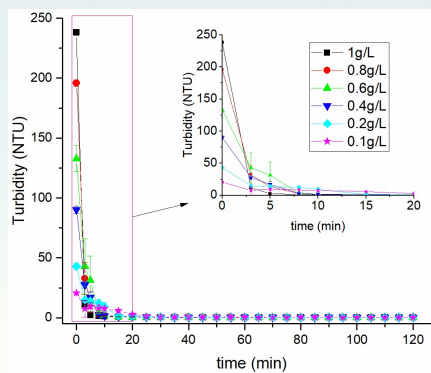
Variation of TMP curve slope with different influent particle concentration



Results—Influencing factors



Variation of filtration resistance with time under different influent particle concentration



Variation of effluent turbidity with time under different influent particle concentration





Conclusion

- ◆ **DM filtration technology** can remove the particles effectively, with low TMP, filtration resistance, and high filtration flux in the DM filtration process.



Conclusion

- ◆ Single blocking model of **cake filtration** can explain the DM formation process with 68 μm and 90 μm mesh, while combined blocking model of **cake-intermediate blocking** performs better. For 158 μm mesh, **cake-standard blocking** model can explain the DM formation process reasonably.



Conclusion

- ◆ **Influent flux** and **influent particle concentration** are found to be able to facilitate the formation of DM layer.



